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Performance of thermal conductivity probes for planetary applications

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Abstract

This work aims to contribute to the development of in situ instruments feasible for space application. Commercial as well as custom made thermal sensors, based on the transient hot wire technique and suitable for direct measurement of the effective thermal conductivity of granular media, were tested for application under airless conditions. The investigated media range from compact specimen of well known thermal conductivity used for calibration of the sensors to various granular planetary analogue materials of different shape and grain size. Measurements were performed under gas pressures ranging from 10^3 hPa down to about 10^{-5} hPa. It was found that for the inspected granular materials the given pressure decrease results in a decrease of the thermal conductivity by about two orders of magnitude. In order to check the ability of custom-made sensors to measure the thermal conductivity of planetary surface layers, detailed numerical simulations predicting the response of the different sensors have also been performed. Both, measurements and simulations, revealed that for investigations under high vacuum conditions (as they prevail e.g. on the lunar surface) the derived thermal conductivity values can significantly depend on the sensor geometry, the axial heat flow and the thermal contact between probe and surrounding material. Therefore in these cases a careful calibration of each particular sensor is necessary in order to obtain reliable thermal conductivity measurements. The custom-made sensors presented in this work can serve as prototypes for payload to be flown on future planetary lander missions, in particular for airless bodies like the Moon, asteroids and comets, but also for Mars.

1 Introduction

The physical property which is in the focus of this work is the thermal conductivity of materials composing the solid near-surface layers of planetary bodies, including the terrestrial planets and their satellites as well as asteroids and comet nuclei. To know

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this property and its variation with depth is of high interest for a correct understanding of solar system objects and their evolution, for several reasons:

- For modeling the thermal evolution of a planet the average heat flux across the surface is the decisive boundary condition. In order to determine this property, (i) the average temperature gradient in the near-surface layer (unaffected by diurnal and seasonal variations) and (ii) the thermal conductivity of the near-surface material must be known (Hofmeister et al., 2007).
- Together with other physical material parameters (e.g. mechanical, electrical, optical) thermal properties control to a high extent the processes taking place on a planetary surface. For example, the activity of comets in response to solar irradiation is strongly influenced by the thermal conductivity of the ice/dust mixture at and below the nucleus' surface (Kömlé, 2005).

Moreover, variations in thermal conductivity can to some extent be used as an indicator for the presence of water or ice, since dry particulate rock (sand) has a significantly smaller thermal conductivity than water-saturated particulates or ice (Incropera et al., 2007). While for Earth direct (in situ) measurements of thermal conductivity and heat flux are relatively simple, because the material is easy to access and there is little limitation concerning mass and power consumption of the instrumentation, the situation is quite different for other planetary bodies. Although there exist also indirect methods to obtain information on the thermal properties of a planetary surface by measuring the emitted IR-flux from an orbiting satellite, such measurements usually need to be supplemented by local measurements to allow proper calibration. Examples for remote measurements are the data obtained for Mars by the *Mars Global Surveyor* Thermal Emission Spectrometer (TES) and the *Mars Odyssey* Thermal Emission Spectrometer (THEMIS) (Mellon et al., 2000).

In situ measurements of thermal properties on planetary bodies other than Earth are still extremely scarce. To date thermal conductivity (and/or heat flux) data exist only for two terrestrial bodies: Moon and Mars. For the Moon the manned space missions

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Apollo 15 (1971) and Apollo 17 (1972) carried a heat flow and physical properties package called ALSEP, which was deposited in pre-drilled boreholes of about 2 m depth on the lunar surface. Both the vertical temperature gradient and the thermal conductivity of the surrounding material was measured (Langseth et al., 1972, 1973).

5 On Mars the first in situ measurements of thermal properties, covering the top view millimeters of the surface were carried out in 2008 by the Thermal and Electrical Conductivity Probe (TECP) on board the lander *Phoenix* (Zent, 2009). A further in situ instrument for measuring thermal properties is the MUlti-PURpose Sensor for Surface and Sub-Surface Science (MUPUS). It is part of the scientific payload on the lander
10 *Philae* on *Rosetta*, a cometary mission on its way to the nucleus of comet Churyumov-Gerasimenko, where it is expected to land in late 2014 (Spohn, 2007).

The perhaps most commonly used method to measure the thermal conductivity of soils and sands is the so-called transient line heat source technique (Wechsler, 1992; Kömle et al., 2007). The basic principle of this method is to insert a constant linear
15 heat source into the sample of interest. Simultaneously the temperature response is measured at or close to the source. The thermal properties of the surrounding material influence the measured temperature increase in a way that under certain conditions the thermal conductivity can be determined from the measured temperature response. Since this method is well approved for thermal conductivity measurements on Earth, it
20 is expedient to use it also on other planetary surfaces. However, to establish successful application of the line heat source method in remote planetary environments demands extensive laboratory testing and modeling work. A comprehensive review of existing prototypes used in or developed for planetary applications was recently given by Kömle et al. (2011).

25 The present work aims to make a contribution towards the development of a robust and reliable in situ thermal conductivity measurement instrument for application on planetary lander missions. Commercial as well as custom-made sensors were tested. A large number of measurements have been performed on several planetary analogue samples in a vacuum chamber at the Space Research Institute (IWF) Graz under

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various pressure conditions. While this paper concentrates mainly on modeling aspects, more details on the results of the performed heat conductivity measurements can be found in Kömle et al. (2010) and in Hütter (2011). To study the behavior of the sensors, numerical models of the measurement configuration for the particular sensors were set up. Special attention was given to problems which are not that significant in terrestrial environments, but can, as was witnessed during this work, become severe in a high vacuum environment. In particular these are axial heat flow along the sensor caused by the electrical connections, high thermal resistance between the sensor and the surrounding sample material, and radiative interaction between sensor and test specimen.

2 Theory of transient thermal conductivity probes

In general the methods for measuring thermal conductivity can be divided into two groups. The steady state techniques on the one hand and the non-steady state techniques on the other. In case of the steady state methods a constant temperature difference is established in the sample. This method demands high complexity of the measurement system and is therefore unsuitable for application in the field or on space missions. The so-called transient techniques generally use a heater of certain geometry embedded in the sample, which is subsequently heated over a defined time interval. At the same time the temperature is measured at or close to the heater. The temperature response depends on the thermal properties of the surrounding medium. Such measurement systems are less complex than steady state methods and are therefore better qualified for field and space applications. The perhaps most commonly used method for measuring the thermal conductivity of soils and sands in situ is the line heat source technique (Wechsler, 1992). This transient method uses an approximately needle shaped heater/sensor combination heated by a controlled electrical power. In the following the theory related to this method is outlined.

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The general approach for the line heat source technique is that of an infinite line source embedded in an infinite, homogeneous, and isotropic medium (Carslaw and Jaeger, 1959). For such cylinder-symmetric boundary value problems the heat conduction equation can be written in the form:

$$5 \quad \frac{1}{\kappa} \frac{\partial T}{\partial t} = \frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \frac{Q(r,t)}{k} \quad (1)$$

valid over the domain $0 < r < \infty$ and $t > 0$. Initial and boundary conditions are given as $T = T_0$ on the domain ($0 < r < \infty, t = 0$) and $T = T_0$ for $r \rightarrow \infty, t > 0$. $Q(r,t)$ denotes a volume heat source [Wm^{-3}]. A general solution can be derived by integral transformation (Hankel-transform, see Özisik, 1989):

$$10 \quad T(r,t) = \int_{\beta=0}^{\infty} \left[\beta J_0(\beta r) \exp(-\kappa \beta^2 t) \left(T_0 \int_{r'=0}^{\infty} r' J_0(\beta r') dr' + \frac{\kappa}{k} \int_{r'=0}^{\infty} r' J_0(\beta r') Q(r',t') dr' \right) \right] d\beta \quad (2)$$

where $J_0(x)$ is the Bessel function of the first kind and zero'th order.

2.1 Continuous line heat source

For the case of a continuous line heat source Q_1 [Wm^{-1}] in the center ($r = 0$) that supplies energy at a constant rate, the volume power density $Q(r,t)$ [Wm^{-3}] can be specified in the form

$$15 \quad Q(r,t) = \frac{Q_1}{2\pi r} \delta(r-0) \quad (3)$$

where $\delta(r-0)$ is the Dirac delta function at the position $r = 0$. Substituting Relation (3) into Eq. (2) leads to the expression for the temperature response due to heat emitted from the line source:

$$20 \quad T(r,t) = T_0 + \frac{Q_1}{4\pi k} \int_{t'=0}^t \frac{1}{(t-t')} \exp\left(-\frac{r^2}{4\kappa(t-t')}\right) dt' = T_0 + \frac{Q_1}{4\pi k} \text{Ei}\left(-\frac{r^2}{4\kappa t}\right) \quad (4)$$

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The expression $-\text{Ei}(-x) = \int_x^\infty \frac{\exp(-u)}{u} du$ in Eq. (4) denotes the *Exponential Integral Function*. This integral can be expressed by a series expansion (Abramowitz and Stegun, 1964) as

$$-\text{Ei}(-x) = -\zeta - \ln x - \sum_{n=1}^{\infty} \frac{(-1)^n x^n}{n n!} = -\zeta - \ln x + x - \frac{1}{4}x^2 + \dots \quad (5)$$

5 where $\zeta = 0.5772$ denotes the Euler constant. For small x -values (equivalent to large values of t) the contributions after the logarithmic term can be neglected and the temperature change can be approximated by

$$T(r, t) = \frac{Q_1}{4\pi k} \left(-\zeta + \ln t + \ln \frac{4\kappa}{r^2} \right) \quad (6)$$

10 Thus the variation of temperature with the natural logarithm of time as the independent variable is

$$\frac{dT}{d \ln t} = \frac{Q_1}{4\pi k} \quad (7)$$

15 In Eq. (7) the temperature rise due to heating depends only on the applied amount of heat Q_1 (heating power per unit length of the line source positioned at $r = 0$), the thermal conductivity k of the surrounding medium, and the time interval used. This approximation gives a linear relation between the temperature change along the line heat source and the natural logarithm of time. From that the thermal conductivity can be derived if heating power and temperature increase as a function of time are known.

2.2 Continuous cylindrical surface source

20 A second problem of interest is that of a continuous cylindrical surface heat source Q_{cyl} [Wm^{-1}] with a radius a (This satisfies the geometry of a thermal conductivity probe

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better than the line heat source ansatz). Following a similar approach as for the line heat source, $Q(r, t)$ is specified as

$$Q(r, t) = \frac{Q_{\text{cyl}}}{2\pi r} \delta(r - a) \quad (8)$$

The solution for the temperature distribution due to a constant continuous cylindrical surface source at $r = a$ can now again be obtained from Eq. (2) by integration (Özisik, 1989):

$$T(r, t) = \frac{Q_{\text{cyl}}}{4\pi k} \int_{t'=0}^t \frac{1}{(t-t')} \exp\left(-\frac{r^2+a^2}{4\kappa(t-t')}\right) I_0\left(\frac{ra}{2\kappa(t-t')}\right) dt' \quad (9)$$

where $I_0(x)$ is the modified Bessel function of zero'th order, which can also be expressed by a series expansion of the form:

$$I_0(x) = \sum_{n=0}^{\infty} \frac{1}{(n!)^2} \left(\frac{x^2}{2}\right)^n = 1 + \left(\frac{x}{2}\right)^2 + \frac{1}{4} \left(\frac{x}{2}\right)^4 + \frac{1}{36} \left(\frac{x}{2}\right)^6 + \dots \quad (10)$$

Using the identity

$$I_0(x) = 1 + [I_0(x) - 1] \quad (11)$$

Equation (9) may be split up into two contributions:

$$T(r, t) = \frac{Q_{\text{cyl}}}{4\pi k} \int_{t'=0}^t \frac{1}{(t-t')} \exp\left(-\frac{r^2+a^2}{4\kappa(t-t')}\right) dt' + \frac{Q_{\text{cyl}}}{4\pi k} \int_{t'=0}^t \frac{1}{(t-t')} \exp\left(-\frac{r^2+a^2}{4\kappa(t-t')}\right) \left[I_0\left(\frac{ra}{2\kappa(t-t')}\right) - 1 \right] dt' \quad (12)$$

The first term of the integral solution given in Eq. (12) is the solution for a line heat source displaced by about the radius of the cylindrical surface source. The second

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term contains the influence stemming from the cylindrical nature of the source. The temperature increase due to heating at the source $r = a$ is obtained as

$$T(t) = \frac{Q_{\text{cyl}}}{4\pi k} \int_{t'=0}^t \frac{1}{(t-t')} \exp\left(-\frac{a^2}{2\kappa(t-t')}\right) dt' + \frac{Q_{\text{cyl}}}{4\pi k} \int_{t'=0}^t \frac{1}{(t-t')} \exp\left(-\frac{a^2}{2\kappa(t-t')}\right) \left[I_0\left(\frac{a^2}{2\kappa(t-t')}\right) - 1 \right] dt' \quad (13)$$

Equation (13) is of interest for thermal conductivity measurements with hollow cylindrical sensors where the temperature response to heating is measured in the close vicinity of the heater. This applies for the LNP01 probe introduced in Sect. 3.

In Fig. 1 the integral solution for a continuous cylindrical surface source is shown along with the two parts the integral can be divided into (see Eq. 13). The parameters used for this graph are those for a measurement with the hollow cylindrical sensor LNP01 in Agar. It can be seen that at small times the solution is dominated by the cylindrical part of Eq. (13) while for times of about 1000 s and larger the term corresponding to a line heat source controls the temperature distribution.

2.3 Consideration of heat source properties

The theory introduced in the previous paragraphs examines infinite samples and infinitely long and thin sensors with therefore negligible thermal properties. The contact between sensor and medium is considered to be ideal. However, this is not the case for real measurement devices. Solutions of the heat equation for the more realistic setup of a finite probe and non-ideal contact between sensor and probe have been developed and discussed amongst others by Jaeger (1956), Blackwell (1954), and de Vries and Peck (1958). The most comprehensive presentation on the theory of cylinder-symmetric heat sources can be found in the classical textbook of Carslaw and Jaeger (1959). In the following the relations given in Jaeger (1956) are outlined. A general integral solution was derived for the problem of a perfectly conducting cylinder

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of a certain radius r_{sen} , heat capacity c_{sen} and density ρ_{sen} , embedded in an infinite medium with known properties. The intersection between sensor and medium is controlled by a contact resistance per unit area given as $1/H$, where H is defined as the contact conductance. The general solution given in Eq. (18) is expressed in terms of the dimensionless parameters τ , α and h , which are defined as:

$$\tau = \frac{\kappa t}{r_{\text{sen}}^2} \quad (14)$$

$$\alpha = \frac{2\pi r_{\text{sen}}^2 \rho c}{S} \quad (15)$$

$$h = \frac{k}{r_{\text{sen}} H} \quad (16)$$

Thermal diffusivity κ , density ρ , specific heat c and thermal conductivity k are the medium properties. S is the heat capacity of the probe per unit length and can be expressed as:

$$S = A_{\text{sen}} c_{\text{sen}} \rho_{\text{sen}} \quad (17)$$

with A_{sen} denoting the cross-section area of the sensor. A dimensionless integral solution can be derived as

$$\frac{T k}{Q_1} = G(h, \alpha, \tau) = \frac{2\alpha^2}{\pi^3} \int_0^\infty \frac{[1 - \exp(-\tau x^2)] dx}{x^3 \Delta(x)} \quad (18)$$

with

$$\Delta(x) = [x J_0(x) - (\alpha - hx^2) J_1(x)]^2 + [x Y_0(x) - (\alpha - hx^2) Y_1(x)]^2 \quad (19)$$

J_0 and J_1 are the Bessel functions of the first kind of order 0 and 1, while Y_0 and Y_1 are Bessel functions of the second kind of order 0 and 1. Approximations for the function

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$G(h, \alpha, \tau)$ can be obtained by series expansions of the integral solution (Eq. 18). Of particular interest is the long time approximation:

$$G(h, \alpha, \tau) = \frac{1}{4\pi} \left[2h + \ln \frac{4\tau}{C} - \frac{(4h - \alpha)}{2\alpha\tau} + \frac{(\alpha - 2)}{2\alpha\tau} \ln \frac{4\tau}{C} \right] \quad (20)$$

where $C = \exp(\zeta) = 1.7811$ with the Euler constant $\zeta = 0.5772$. For the limiting case of a very thin sensor and vanishing contact resistance Relation (20) becomes Relation (6). The given equations can be used to simulate the temperature response due to heating for known properties of sample and sensor.

3 Measurement probes

The geometry and principle of the transient hot wire technique as outlined in the previous sections allows bottom-of-the-line field application. This method has been assigned for a broad application range. The commercial needle sensors TP02 and TP08 investigated in this work are suitable for various granular materials like sands, soils and powders. Such a needle-shaped sensor could be placed at the tip of an robotic arm, as the thermal and electrical conductivity probe TECP on the Mars polar lander *Phoenix*. However, for this application a sensor of several centimeter length should be robust and resistant against bending. The TP02 and TP08 do not fulfil this requirement. During investigation of the particulate rock material with grain sizes larger than one millimeter it was noted that the commercial sensors easily got stuck and tended to be deformed by bending. The more robust prototypes LNP02 and LNP03 were not affected by this problem and are therefore more suitable for granular rock.

The third kind of sensor investigated is the LNP01, which is a large hollow cylindrical sensor. Such a sensor could be implemented into a drilling rod. Further this sensor concept is similar to the thermal property measurement system implemented in the hull of the HP³-instrument, a mole-type probe for subsurface exploration¹. All sensors used

¹http://www.dlr.de/dlr/en/desktopdefault.aspx/tabid-10255/365_read-818

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sensor remains hollow (optionally it can be filled up by sample material). For differential temperature measurement thermocouple junctions are located in the middle and near the bottom end of the LNP01, respectively. The power for heating is supplied by an external constant current source which allows free adjustment of the heating power.

3.3 Short and robust prototypes (LNP02, LNP03)

The LNP02 and LNP03 sensors, shown in Fig. 4, are of comparable size as the commercial TP08 thermal conductivity probe, but more robust and can hardly be bended when pushed into granular or slightly cohesive material. The LNP03 has an diameter of 3.5 mm, while the LNP02 has an mean diameter of 4.5 mm. Both sensors have a length of 100 mm and are heated over the whole length by a constantan heating wire. The only difference between the two types is that the former has a circular cross section while the latter is shaped similar to an auger drill. For each probe the temperature response to heating is measured by three temperature dependent resistors (Pt1000). These are placed at the tip, the middle and the base of the sensor. The temperature measurement is done in a four wire configuration.

3.4 Constraints

Naturally the thermal conductivity probes used for real measurements deviate from the theoretical assumption for a transient line heat source as outlined in Sect. 2. They have finite dimensions and non-negligible properties. The investigated samples are, especially in the case of laboratory measurements, of limited size and the contact between measurement probe and specimen is also not ideal. These limitations lead to some constraints that have to be considered.

3.4.1 Transient time after onset of heating

The time period t_{trans} is an estimate for the duration of the nonlinear part of the temperature versus $\ln t$ curve after the onset of heating. This nonlinear part is mainly due

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to the initial heating of the finite sensor volume, since the heat wave has to propagate through the sensor material first. It also depends on the thermal properties of the surrounding medium, because for a proper measurement an adequate specimen volume has to be sampled. Additionally the transient time is influenced by the contact resistance. It was shown by Vos (1955) and Goodhew and Griffiths (2004) that the minimum nonlinear time period can be estimated as

$$t_{\text{trans}} \geq \frac{50 r_{\text{sen}}^2}{4\kappa_{\text{sample}}} \quad (21)$$

Relation (21) is valid for uniform heating of a thin cylindrical sensor like e.g. the TP02. However, for the LNP01 sensor, that has the shape of a hollow cylinder, an effective sensor radius has to be defined (Kömle et al., 2010). This is done by deriving an equivalent cylinder radius for the volume of the hollow cylinder. The volume of the hollow cylinder V_{hc} is given by

$$V_{\text{hc}} = (r_{\text{O}}^2 - r_{\text{I}}^2)\pi l \quad (22)$$

where l is the length of the sensor and r_{I} and r_{O} are the inner and outer radius. The volume of the equivalent full cylinder V_{c} is

$$V_{\text{c}} = r_{\text{eq}}^2 \pi l \quad (23)$$

with r_{eq} being the equivalent radius. Equating (22) and (23) leads to the following expression for the equivalent radius:

$$r_{\text{eq}} = \sqrt{(r_{\text{O}}^2 - r_{\text{I}}^2)} \quad (24)$$

For the LNP01 sensor one obtains $r_{\text{eq}} = 4.7$ mm. The transient times as calculated by Eq. (21) for the different sensors and a selection of different materials are plotted in Fig. 5 (top panel). As expected, the longest transient times were derived for the largest sensor and the shortest transient times were found for the smallest sensor.

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First an initial phase after the onset of heating, which is dominated by the self-heating of the sensor and contact resistance, is observed. This is followed by a section where the temperature versus natural logarithm of time data are linear. This is the part needed for the determination of the thermal conductivity, if the long time approximation given in Eq. (6) is used. From the slope of the temperature versus $\ln t$ data, thermal conductivity can be calculated by using Eq. (7). In the adjacent third part the data are nonlinear again. In this domain, effects of finite sample dimensions and axial errors become important and the data can no longer be evaluated by using Eq. (7). An increase of the measurement curve in the third part as shown in Fig. 6 can, for example, be observed if the wall of the sample container is reached by the heat wave and the conductivity of the container material is lower than that of the sample. A decrease in this part is observed if convection starts to play a role or if the conductivity of the container wall is higher than the sample conductivity.

During a measurement the temperature versus time series with and without heating is collected by a data logger suitable for the particular sensor. From the logged temperature-time data, the heating current, and the heater resistance the thermal conductivity is determined. The information about the samples allows to estimate transient and maximum measurement times, which subsequently can be used to narrow down the part of the measurement curve used for evaluation. Finally the data can be evaluated in three ways that are in the following outlined in more detail.

3.5.1 Linear regression

From the linear part of the temperature versus natural logarithm of time data the thermal conductivity is calculated using a linear fit of the form

$$T(t) = A + B \ln t \quad (26)$$

where the coefficient B corresponds to the right side of Eq. (7) and therefore the thermal conductivity can be derived as

$$k = \frac{P}{4\pi B} \quad (27)$$

where P is the constant heating power per unit length applied to the sensor during the measurement. In general the linear part to be used for the evaluation lies in between the nonlinear sections as sketched in Fig. 6. Thus the challenge of the data interpretation lies in identifying the linear part of the curve. For this purpose the transient time t_{trans} , giving the minimum duration of the nonlinear part after onset of heating, and the maximum measurement time t_{max} , giving the time after which the heat wave reaches the sample boundary, are used as criteria to constrain the evaluation interval. On the time interval defined by these two boundaries a linear least squares fit is performed.

3.5.2 Successive linear regression

Since t_{trans} and t_{max} can only be estimated, they might not always apply to the measured data. The uncertainties for transient and maximum time lie in the estimates available for the sample diffusivity and the usually unknown magnitude of the contact resistance. Furthermore axial losses or the onset of convection could reduce the duration of the linear part. To minimize errors in the determined thermal conductivity arising from these effects, successive linear regression can be used.

For this purpose the part of the measurement curve starting from t_{trans} and the corresponding temperature is divided into sub-intervals. On these curve-sections linear least squares fits are performed. For the measurements evaluated a fit interval of 10 measurement points (this corresponds generally to a time interval of 10 s in our data sets) was chosen. It was assumed that the majority of the successively determined slopes/conductivities can be derived from the linear part of the measurement curve. Thus the median of these values should give a good estimate for the conductivity.

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3.5.3 Nonlinear regression

A nonlinear long time approximation for the heating curve, considering a probe with finite diameter and non-negligible properties and contact resistance between sample and probe, has been used for evaluation for example by Jones (1988), Koski and McVey (1983) and Erbas (2001). This relation is a better approximation of the measurement situation and therefore should yield better values. The regression equation has the form

$$T(t) = A + B \ln t + C \frac{\ln t}{t} + D \frac{1}{t} \quad (28)$$

where terms of the order $(1/t^2)$ and higher are neglected. The coefficients in Eq. (28) can be expressed as follows

$$A = \frac{P}{4\pi k} \left[\ln \left(\frac{4\kappa}{r_{\text{sen}}^2} \right) - \zeta + \frac{2k}{r_{\text{sen}} H} \right] \quad (29)$$

$$B = \frac{P}{4\pi k} \quad (30)$$

$$C = \frac{P}{4\pi k} \frac{r_{\text{sen}}^2}{2\kappa} \left(1 - \frac{\kappa S}{\pi r_{\text{sen}}^2 k} \right) \quad (31)$$

$$D = \frac{P}{4\pi k} \frac{r_{\text{sen}}^2}{2\kappa} \left\{ \ln \left(\frac{4\kappa}{r_{\text{sen}}^2} \right) + (1 - \zeta) - \frac{\kappa S}{\pi r_{\text{sen}}^2 k} \left[\ln \left(\frac{4\kappa}{r_{\text{sen}}^2} \right) - \zeta + \frac{2k}{r_{\text{sen}} H} \right] \right\} \quad (32)$$

The regression Eq. (28) is equivalent to Eq. (20).

4 Numerical modeling of the sensor response

In order to better understand the temperature response of the sensors, the three types of line heat sensors investigated in this work were also modeled with the finite element

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- Sample setting (1): very low sample conductivity: $k = 0.002 \text{ Wm}^{-1} \text{ K}^{-1}$, $\rho = 1510 \text{ kgm}^{-3}$, $c = 633 \text{ Jkg}^{-1} \text{ K}^{-1}$, $H = 1250 \text{ Wm}^{-2} \text{ K}^{-1}$ (good contact), $H = 12.5 \text{ Wm}^{-2} \text{ K}^{-1}$ (poor contact), $\varepsilon_{\text{sen}} = 1.0$, $\varepsilon_{\text{mat}} = 1.0$
- Sample setting (2): low sample conductivity: $k = 0.02 \text{ Wm}^{-1} \text{ K}^{-1}$, $\rho = 1510 \text{ kgm}^{-3}$, $c = 633 \text{ Jkg}^{-1} \text{ K}^{-1}$, $H = 1250 \text{ Wm}^{-2} \text{ K}^{-1}$ (good contact), $H = 12.5 \text{ Wm}^{-2} \text{ K}^{-1}$ (poor contact), $\varepsilon_{\text{sen}} = 1.0$, $\varepsilon_{\text{mat}} = 1.0$
- Sample setting (3): moderate sample conductivity: $k = 0.2 \text{ Wm}^{-1} \text{ K}^{-1}$, $\rho = 1510 \text{ kgm}^{-3}$, $c = 633 \text{ Jkg}^{-1} \text{ K}^{-1}$, $H = 1250 \text{ Wm}^{-2} \text{ K}^{-1}$ (good contact), $H = 12.5 \text{ Wm}^{-2} \text{ K}^{-1}$ (poor contact), $\varepsilon_{\text{sen}} = 1.0$, $\varepsilon_{\text{mat}} = 1.0$

The values chosen for material density and specific heat are those of glass beads of 0.25–0.5 mm grain size (Hütter, 2011, p. 55). Thus the results of the numerical simulations can be used to analyze the measurement results for those glass beads. The value of contact conductance used for poor contact was taken from Kömle et al. (2008) where it was derived for lunar conditions. As *good contact* a hundred times better contact conductance was considered. The thermal emissivities of sensor and sample required for radiative interaction were chosen to be those of a black body. In this way the maximum influence of the radiation heat transfer can be assessed.

The applied sample parameters correspond to a thermal diffusivity of $2.1 \times 10^{-9} \text{ m}^2 \text{ s}^{-1}$ for the very low conductivity, $2.1 \times 10^{-8} \text{ m}^2 \text{ s}^{-1}$ for the low conductivity and $2.1 \times 10^{-7} \text{ m}^2 \text{ s}^{-1}$ for the moderate conductivity. In Table 3 the transient and maximum measurement times derived for the examined sensors and sample settings are listed.

The heating powers applied for the different sensor types and scenarios were chosen in dependence of the estimated sample thermal conductivity. The criterion was that the temperature rise in response to heating should be no more than a few degrees over the entire measurement period. In case of the very low conductivity setting this led to extremely low heating powers of 10^{-3} W for all sensors. This matches the powers used in the Apollo heat flow experiments (Langseth et al., 1972, 1973).

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temperature increase for the setting of pure conduction and axial losses via the cables (No. 3 and No. 4) is somewhat higher. The case of pure radiative heat transport between sensor and sample (No. 5) without cables yields a temperature curve in between the data obtained for pure conduction with and without axial heat flow allowed.

In the semi-logarithmic representation given in Fig. 9b clear differences in the shape of the temperature curves can be noticed. The data was evaluated using the three methods outlined in Sect. 3.5. For each scenario first the interval specified by the transient and maximum measurement time was evaluated. In addition also an early time interval of the measurement curve was evaluated. For the settings No. 1 and No. 2 both evaluation intervals led to values close to the prescribed sample conductivity. For the early time evaluation interval the methods of linear regression and successive linear regression give higher conductivities than for the time period specified by t_{trans} and t_{max} .

Settings No. 3 and No. 4, where axial heat flow is considered, yields differences in the determined thermal conductivity dependent on the used evaluation method. Best values (closest to sample conductivity) are obtained with the nonlinear fit method, while the other methods deliver higher values. Since the measurement curves for these scenarios depict a bend, an additional interval covering the late measurement times was inspected. From this time period slightly higher thermal conductivities than the sample conductivity were derived by all three methods. The settings involving radiation all yielded significantly higher conductivities than the sample conductivity. From the obtained results several conclusions can be drawn:

- Axial losses via the base and electrical wires result in a smaller temperature increase and a bend of the measurement curve in the semi-logarithmic presentation dividing it in two parts. Separate analysis of these parts gives higher conductivities for the first part and conductivities close to the true sample conductivity for the second part.

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- For LNP01 measurements in specimen of very low conductivity the development of axial heat flow leads to a smaller overall temperature increase. As for the TP02 the measurement curves depict a different shape of the temperature versus $\ln t$ plot. Axial losses result in higher determined conductivities.
- Differences in contact resistance cause a hardly noticeable shift of the curve.
- In contrast to the results for the TP02 the measurement curves for settings involving radiative heat transport do not appear significantly different in shape and the conductivities derived from these temperature responses are similar to those without radiation.

4.3.2 Setting (2): low sample conductivity ($k = 0.02 \text{ Wm}^{-1} \text{ K}^{-1}$)

The setting of a low sample thermal conductivity was investigated for measurement periods of 36 h. The temperature time series derived for the different scenarios are displayed in Fig. 14. As for the TP02 a split up of the measurement curves dependent on the investigated scenarios can be observed. The highest temperature increase was found for the setting of pure radiation heat transport (No. 5) and the lowest for the scenario of good contact between sensor and sample and axial heat flow happening (No. 4). The data was evaluated in the time interval specified by transient and maximum measurement time and an early time interval. The conductivities determined for the early time interval are considerable higher than those determined from the interval given by t_{trans} and t_{max} . Further the conductivities calculated from the early time interval depict a dependence on contact resistance. Good contact leads to higher conductivities than poor contact.

- Axial heat flow influences the measured temperatures in way that leads to higher evaluated conductivities.
- Differences in contact resistance produce modifications of the temperature response at early measurement times that lead to different conductivities if

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4.4.1 Setting (1): very low sample conductivity ($k = 0.002 \text{ Wm}^{-1} \text{ K}^{-1}$)

The simulations for LNP03 measurements in a sample of very low conductivity deliver measurement curves similar to those obtained for simulated TP02 measurements in a material of very low conductivity. Measurement periods of 36 h were simulated. The derived temperature responses and their semi-logarithmic representations are shown in Fig. 17. However, no upward bending of the temperature versus time series in the semi-logarithmic plot as for the TP02 was found. Nevertheless the data are split in three groups. The one with the highest temperature increase corresponds to the settings in which axial heat flow is not included (No. 1, No. 2 and No. 5). The two curves with the lowest temperature increase are related to the scenarios considering pure conduction and axial heat flow (No. 3 and No. 4). The data was evaluated in the time period specified by t_{trans} and t_{max} . The conductivities obtained from data of settings including axial heat flow are at least ten times larger than the conductivities calculated from the data related to other scenarios. The following conclusions can be drawn:

- Axial heat flow modifies the data such that the evaluation leads to significantly higher conductivities than the true sample conductivity.
- A difference in contact resistance causes a parallel shift of the curves in the semi-logarithmic representation for times larger than 10 000 s. This behavior was also found for TP02 and LNP01.
- Radiative heat transfer leads to a somewhat higher temperature increase as the scenarios considering conduction and axial losses only.

4.4.2 Setting (2): low sample conductivity ($k = 0.02 \text{ Wm}^{-1} \text{ K}^{-1}$)

For the setting of a low sample conductivity measurements of 36 h were simulated. Figure 18 shows the temperature responses derived for the different settings. Similar as for the TP02 an even split up of the measurement curves can be observed. The

strongest modification. Thus, if the radiative interaction between sensor and sample would be replaced by a corresponding contact resistance, it would be even higher than the contact resistance used for poor contact in this work.

5.4 Evaluation methods

- 5 The nonlinear fit method is the most stable evaluation method and gives the best values also for early time intervals. Influences of too short measurement times and axial heat flow are most severe for the method of linear regression and successive linear regression. Thus the best evaluation technique of choice is the nonlinear fit method.

6 Conclusions

- 10 In this work sensors suitable for the measurement of the thermal conductivity of soils in situ were investigated for application on surfaces of extraterrestrial bodies like the Moon or Mars. For this purpose thermal conductivity tests on various granular materials under differing pressure conditions have been performed with five different sensors based on the transient line heat source technique. These were two commercial (TP02, TP08) and three custom made probes (LNP01, LNP02, LNP03). Furthermore numerical models of the applied sensor types were set up, in which measurement scenarios could be studied that were not realizable with the equipment at hand. The measurement and simulation data was analyzed in terms of thermal conductivity using three different evaluation methods, namely linear regression of a predefined interval of the measurement curve, successive linear regression and nonlinear regression.

- 20 First all sensors were tested under laboratory conditions on materials of well known thermal conductivity. By and large all sensors gave consistent results, only the LNP03 and LNP02 probes tend to yield too high thermal conductivities. After that measurements were done on granular materials at air pressure. The obtained data yielded consistent and reliable results. It follows that the particulate specimen investigated in Hütter (2011) and Kömle et al. (2010) have an effective thermal conductivity in the order of $10^{-1} \text{ W m}^{-1} \text{ K}^{-1}$ at the normal gas pressure of 10^3 hPa . On many extraterrestrial

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surfaces reduced pressure conditions are prevailing. Thus thermal conductivity measurements were performed on granular material under varying pressures ranging from air pressure of 10^3 hPa down to high vacuum of 10^{-4} hPa. All derived data showed the well known decrease of the effective thermal conductivity with decreasing pressure. However, for pressures below 1 hPa, the values obtained from the different sensors for the same material were inconsistent, depicting a dependency on the used sensor.

This problem was accessed in more detail with the numerical simulations of measurements with the particular sensors in material of varying conductivity. From the results it can be seen that for vacuum conditions axial losses play a significant role, while at ambient conditions contact resistance is the influencing factor. *Thus the results of the numerical simulations suggest that the difference in evaluated thermal conductivity depending on the used sensor at high vacuum is caused by axial losses and too short measurement periods.* The model calculations for the different sensors showed that modifications of the measurement curves due to axial losses become most severe for very low conductivities in the range of $10^{-3} \text{ Wm}^{-1} \text{ K}^{-1}$, which is the case under high vacuum conditions. Under high vacuum conditions very low heating powers are needed. Furthermore the necessary measurement times, especially for large sensors in samples of very low conductivity as particulates in vacuum, are up to several days. To fulfill these needs, appropriate data loggers and software, respectively, have to be used. Moreover, the very low sample conductivities produce severe axial losses in the measurement probes which lead to significant errors in the evaluated conductivity. This is an important point that needs to be addressed in future work.

Further it follows that thermal conductivity measurements on airless bodies like the Moon using methods based on the transient line heat source technique are strongly influenced by axial losses and need special treatment. For bodies like Mars, where the ambient pressure ranges from 6–10 hPa the measurements and simulations reported in this work indicate that such problems would not occur.

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Table 1. Maximum and minimum measurement times estimated for the different sensors when used in various calibration materials.

Sensor	Sample	r_{sample} [m]	k_{sample} [m ² s ⁻¹]	t_{trans} [s]	t_{max} [s]	
$d_{\text{sen}} = 1.5 \times 10^{-3}$ m	TP02	Agar	0.135	14×10^{-8}	50	19 000
		Teflon	0.050	12×10^{-8}	59	3030
		PMMA	0.030	10×10^{-8}	70	1350
		Glycerin	0.040	09×09^{-8}	78	2670
$d_{\text{sen}} = 1.3 \times 10^{-3}$ m	TP08	Agar	0.135	14×10^{-8}	38	19 340
		Teflon	0.050	12×10^{-8}	44	3040
		PMMA	0.030	10×10^{-8}	53	1290
		Glycerin	0.040	09×09^{-8}	59	2580
$d_{\text{sen}} = 9.4 \times 10^{-3}$ m	LNP01	Agar	0.135	14×10^{-8}	1972	18 200
		Teflon	0.050	12×10^{-8}	2300	2570
		PMMA	0.030	10×10^{-8}	2760	3080
		Glycerin	0.040	09×09^{-8}	3068	1070
$d_{\text{sen}} = 4.5 \times 10^{-3}$ m	LNP02	Agar	0.135	14×10^{-8}	452	18 900
		Teflon	0.050	12×10^{-8}	527	2850
		PMMA	0.030	10×10^{-8}	633	1160
		Glycerin	0.040	09×09^{-8}	703	2380
$d_{\text{sen}} = 3.5 \times 10^{-3}$ m	LNP03	Agar	0.135	14×10^{-8}	273	19 000
		Teflon	0.050	12×10^{-8}	319	2910
		PMMA	0.030	10×10^{-8}	382	1200
		Glycerin	0.040	09×09^{-8}	425	2440

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Table 2. Measurement scenarios addressed for each of the three sensor geometries and sample conductivities.

No	contact	cable	radiation
1	poor	no	no
2	good	no	no
3	poor	yes	no
4	good	yes	no
5	no	no	yes
6	no	yes	yes
7	no	yes	yes

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Table 4. Parameters used for the different domains of the TP02-model.

Domain	T_{initial} [K]	c [Jkg ⁻¹ K ⁻¹]	ρ [kgm ⁻³]	k [Wm ⁻¹ K ⁻¹]
(1): electrical wires of the sensor (material: copper)	297	385	8700	400
(2): insulation of the wires (material: Teflon (PTFE))	297	960	2200	0.25
(3): plastic protection of the wires leaving the base (material: PVC)	297	960	1380	0.15
(4), (5), (6): sensor base, heated part of the needle and unheated part of the needle (material: stainless steel)	297	500	7900	16

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Table 6. Parameters used for the different domains of the LNP03-model.

Domain	T_{initial} [K]	c [Jkg ⁻¹ K ⁻¹]	ρ [kgm ⁻³]	k [Wm ⁻¹ K ⁻¹]
(1): electrical wires of the sensor (material: copper)	297	385	8700	400
(2): plastic protection of the wires leaving the base (material: PVC)	297	900	1380	0.15
(3), (5): sensor base and unheated part of the needle (material: stainless steel)	297	500	7900	16
(4): constantan heating wire	297	410	8900	49

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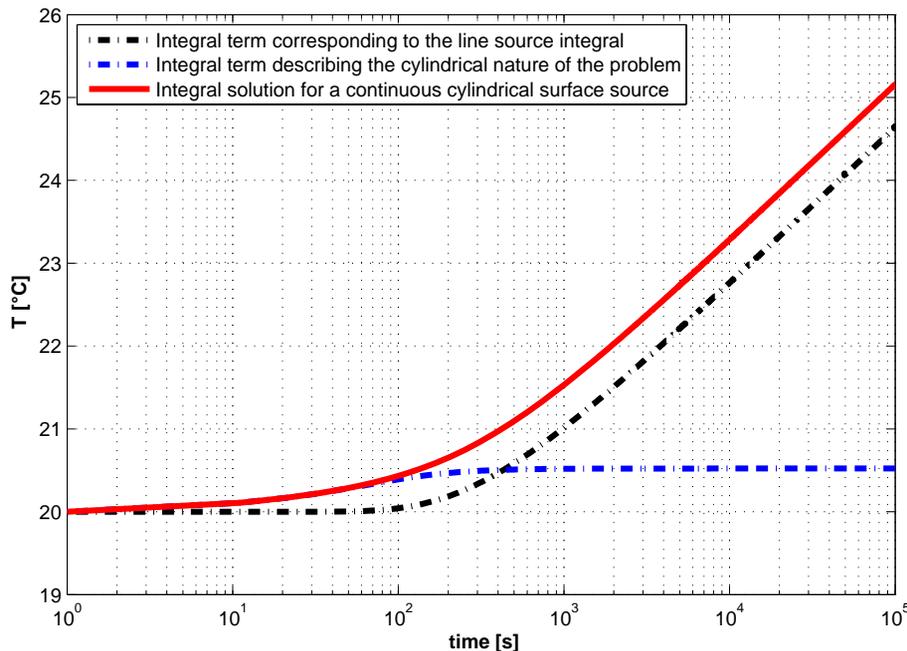


Fig. 1. Integral solutions for a continuous cylindrical surface source. The used parameters match those of a measurement with LNP01 performed in Agar. ($r_1 = 0.0075$ mm; $Q_{\text{cyl}} = 6.15$ Wm $^{-1}$; $k = 0.6$ Wm $^{-1}$ K $^{-1}$; $\kappa = 11 \times 10^{-8}$ m 2 s $^{-1}$).

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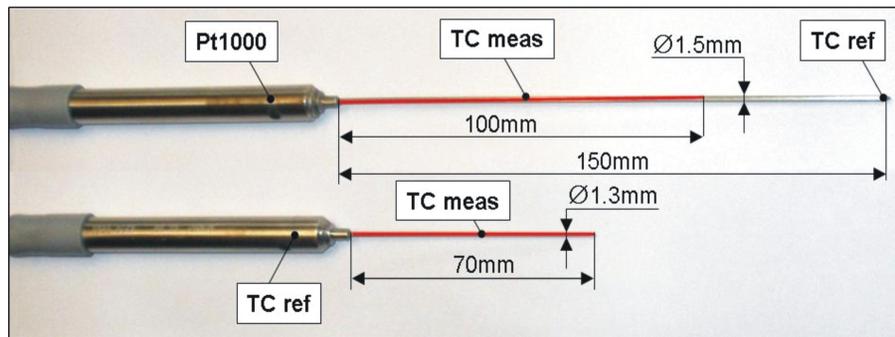


Fig. 2. The commercial TP02 (long needle) and TP08 (short needle) thermal conductivity probes produced by the Dutch company Hukseflux. The heated part is indicated in red.

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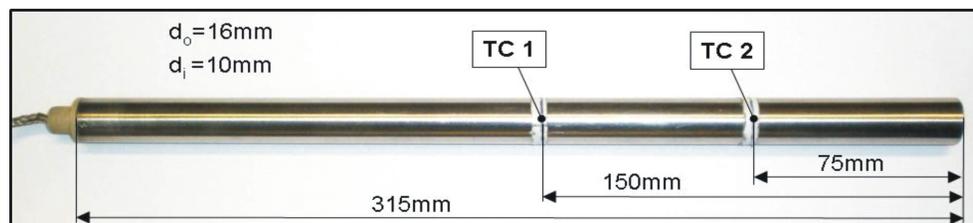


Fig. 3. The thermal conductivity probe prototype LNP01. This hollow cylindrical sensor is heated over its whole length.

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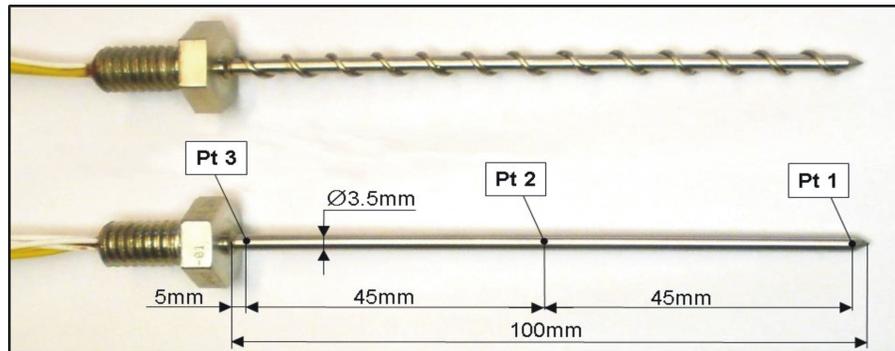


Fig. 4. The LNP02 (needle with winding) and LNP03 (plane needle) prototype.

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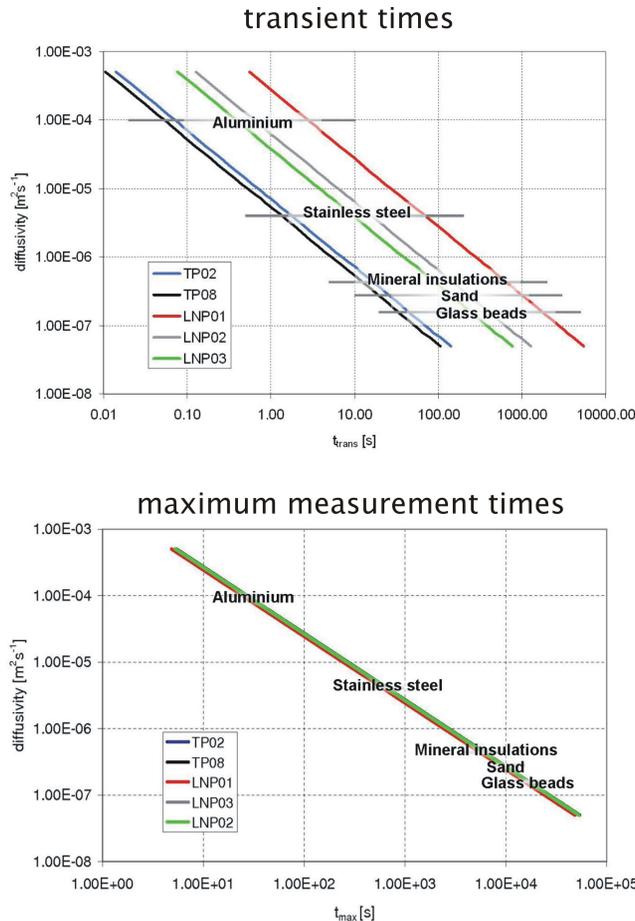


Fig. 5. Transient times and maximum measurement times calculated for the five investigated thermal probes using a diffusivity range from $\kappa = 8 \times 10^{-4} \text{ m}^2 \text{ s}^{-1}$ to $\kappa = 5 \times 10^{-8} \text{ m}^2 \text{ s}^{-1}$.

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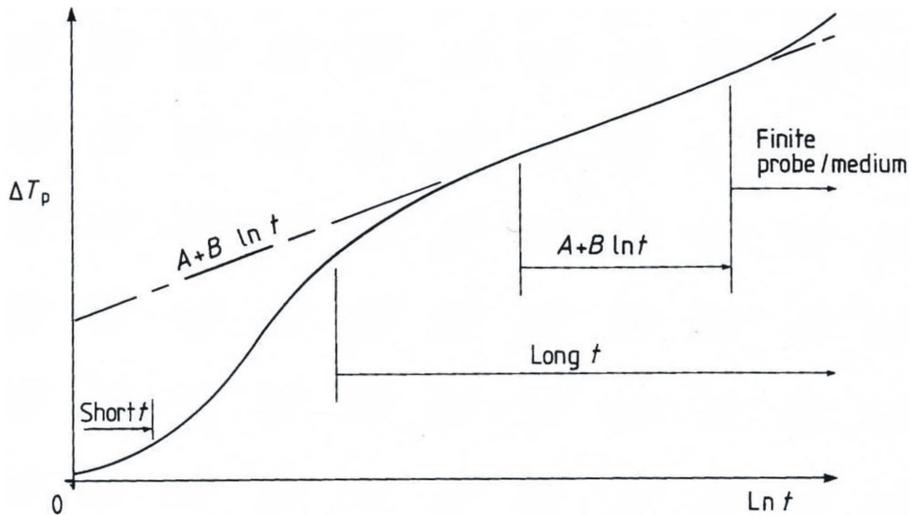


Fig. 6. Qualitative heating curve measured with a line heat sensor (after Jones, 1988 [29]).

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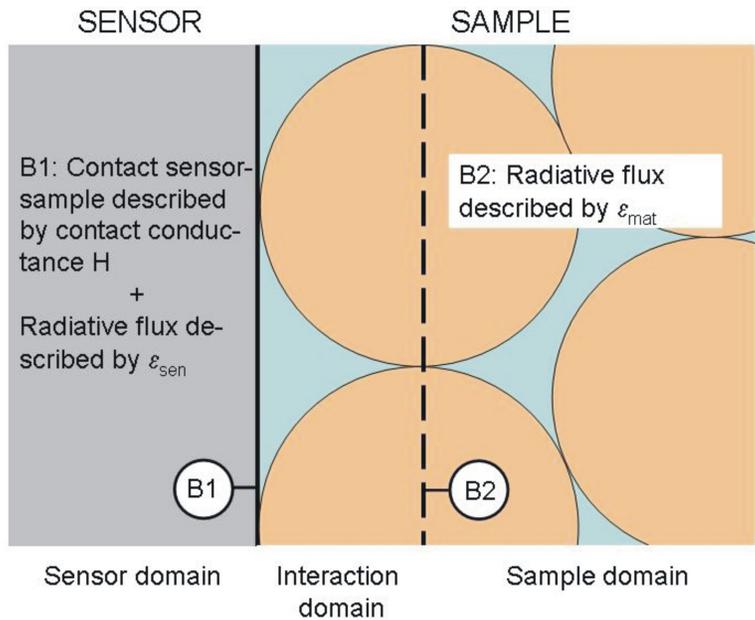


Fig. 7. Schematic of the heat transfer mechanisms between sensor and sample.

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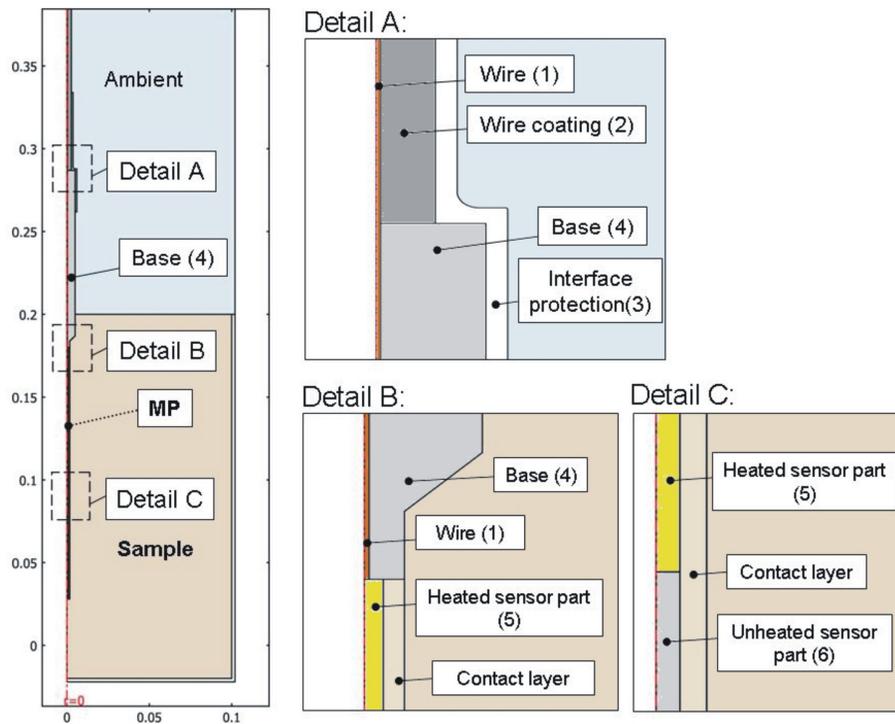


Fig. 8. Model of the TP02 sensor embedded in a sample.

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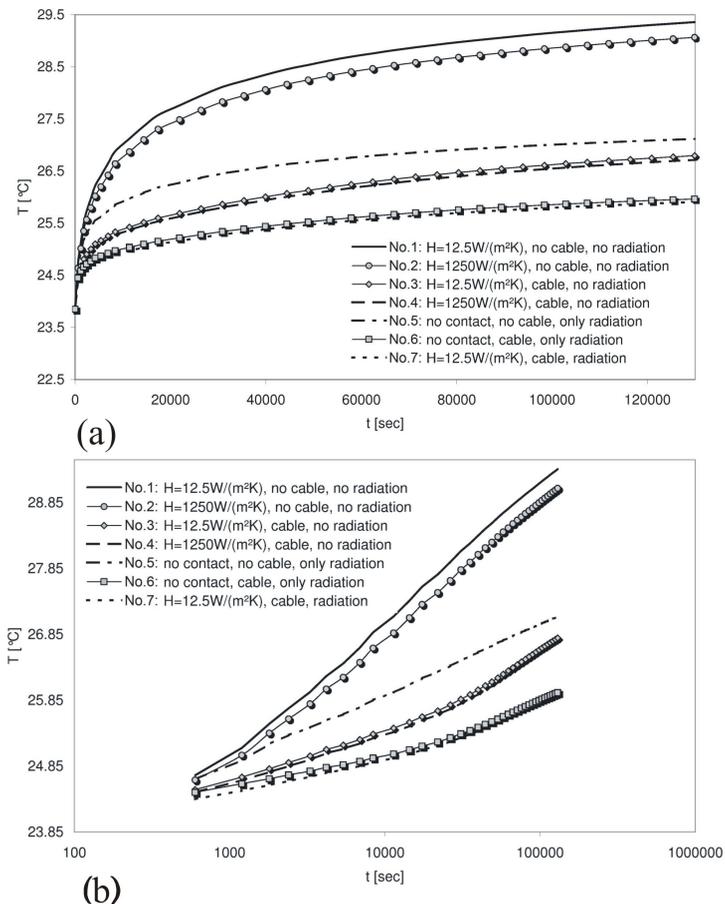


Fig. 9. Temperature response of the commercial TP02-sensor at the measurement point due to heating in a very low conductivity sample with $\lambda = 0.002\text{Wm}^{-1}\text{K}^{-1}$. **(a)** Temperature versus time on a linear time scale. **(b)** Temperature versus time on a logarithmic time scale.

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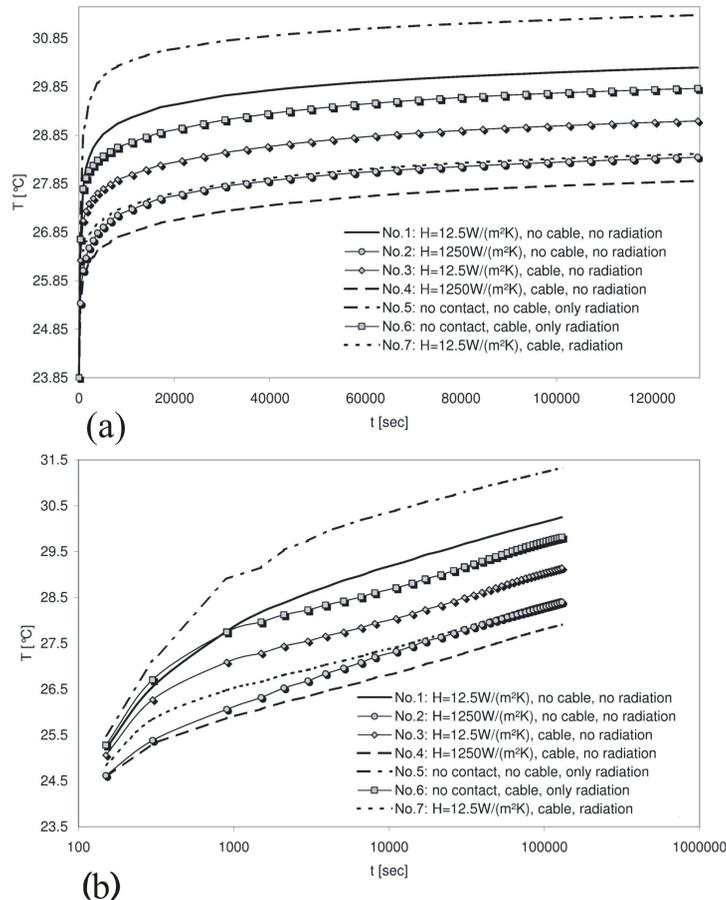


Fig. 10. Temperature response of the commercial TP02-sensor at the measurement point due to heating in a low conductivity sample with $\lambda = 0.02 Wm^{-1} K^{-1}$. **(a)** Temperature versus time on a linear time scale. **(b)** Temperature versus time on a logarithmic time scale.

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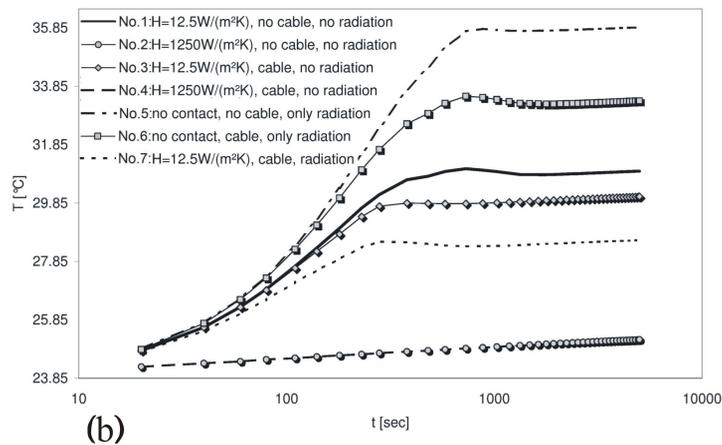
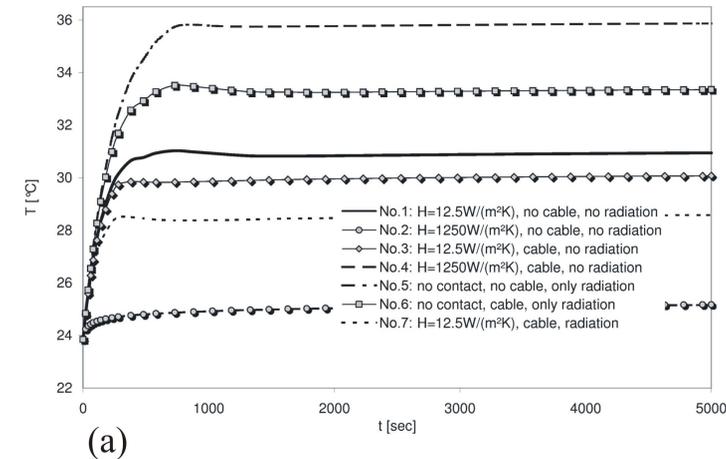


Fig. 11. Temperature response of the commercial TP02-sensor at the measurement point due to heating in a moderate conductivity sample with $\lambda = 0.2 \text{ W m}^{-1} \text{ K}^{-1}$. **(a)** Temperature versus time on a linear time scale. **(b)** Temperature versus time on a logarithmic time scale.

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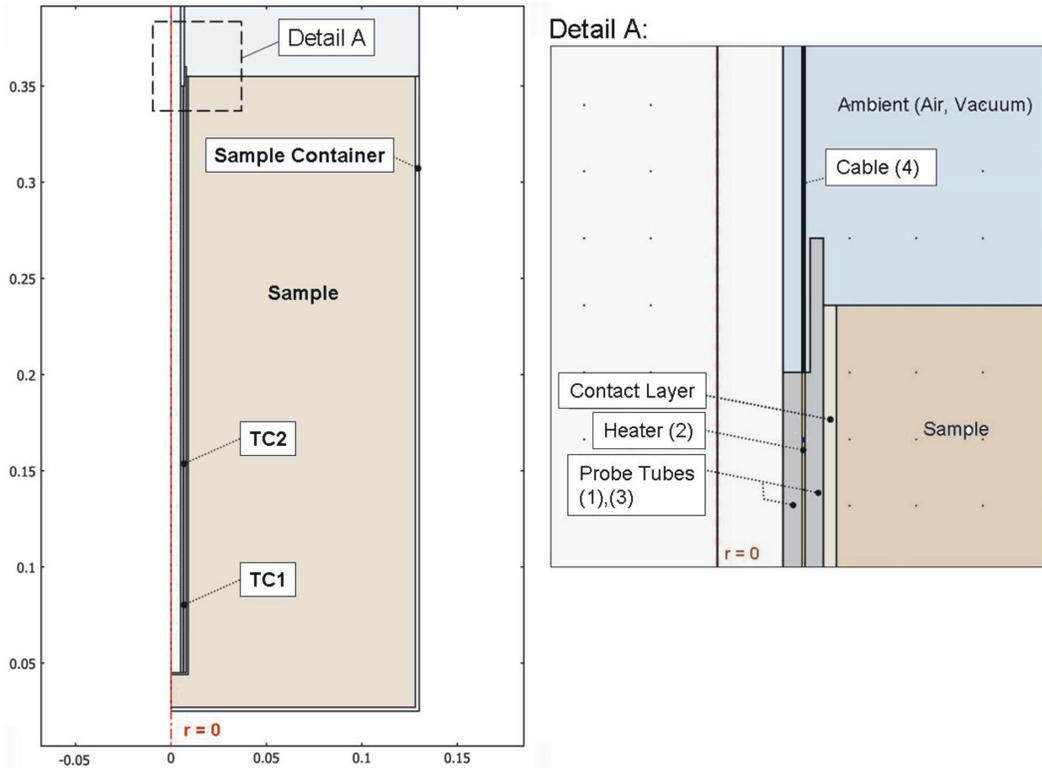


Fig. 12. Model of the LNP01-sensor embedded in a sample.

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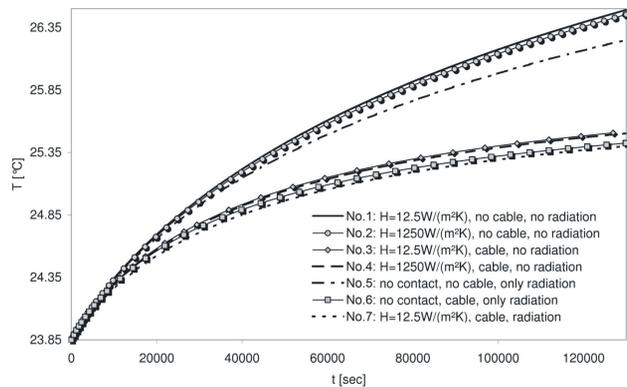
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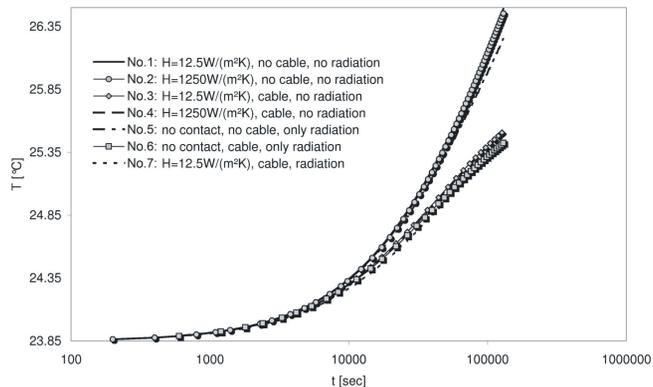
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(a)



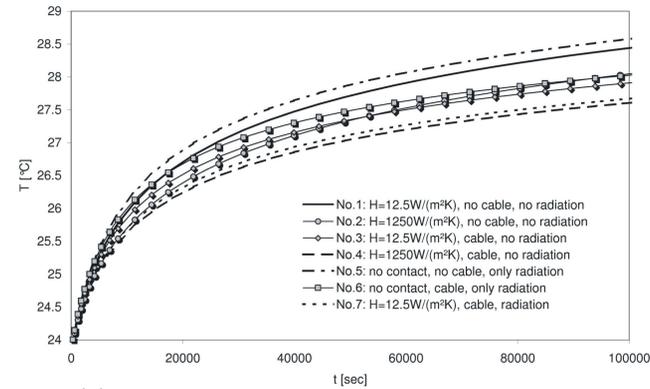
(b)

Fig. 13. Temperature response of the hollow cylindrical LNP01-sensor at the measurement point due to heating in a very low conductivity sample with $\lambda = 0.002 \text{ Wm}^{-1} \text{ K}^{-1}$. **(a)** Temperature versus time on a linear time scale. **(b)** Temperature versus time on a logarithmic time scale.

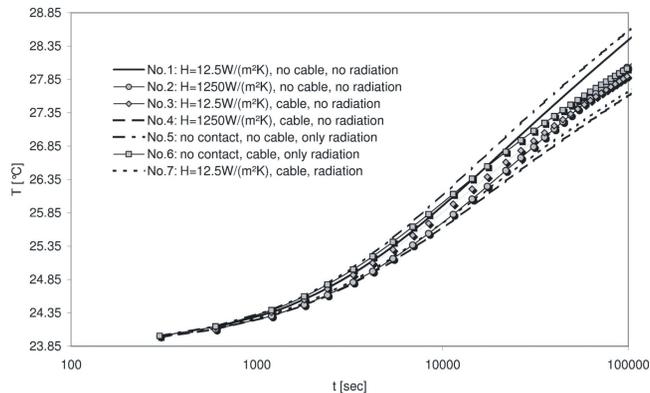
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(a)

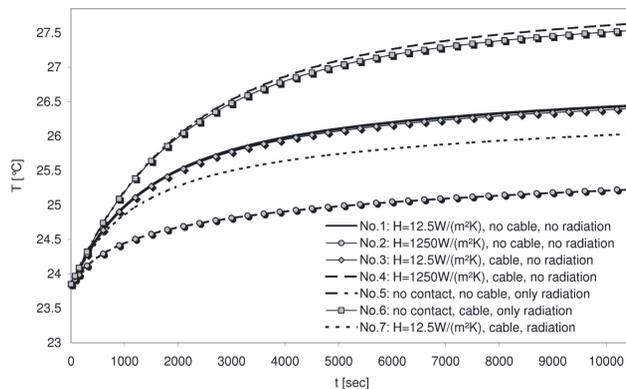


(b)

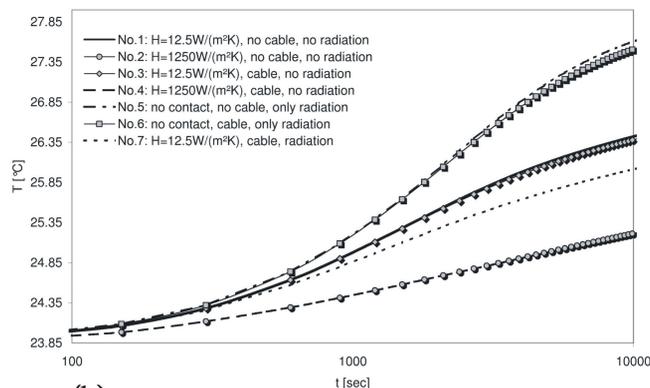
Fig. 14. Temperature response of the hollow cylindrical LNP01-sensor at the measurement point due to heating in a low conductivity sample with $\lambda = 0.02 \text{ Wm}^{-1} \text{ K}^{-1}$. **(a)** Temperature versus time on a linear time scale. **(b)** Temperature versus time on a logarithmic time scale.

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(a)



(b)

Fig. 15. Temperature response of the hollow cylindrical LNP01-sensor at the measurement point due to heating in a moderate conductivity sample with $\lambda = 0.2 \text{ Wm}^{-1} \text{ K}^{-1}$. **(a)** Temperature versus time on a linear time scale. **(b)** Temperature versus time on a logarithmic time scale.

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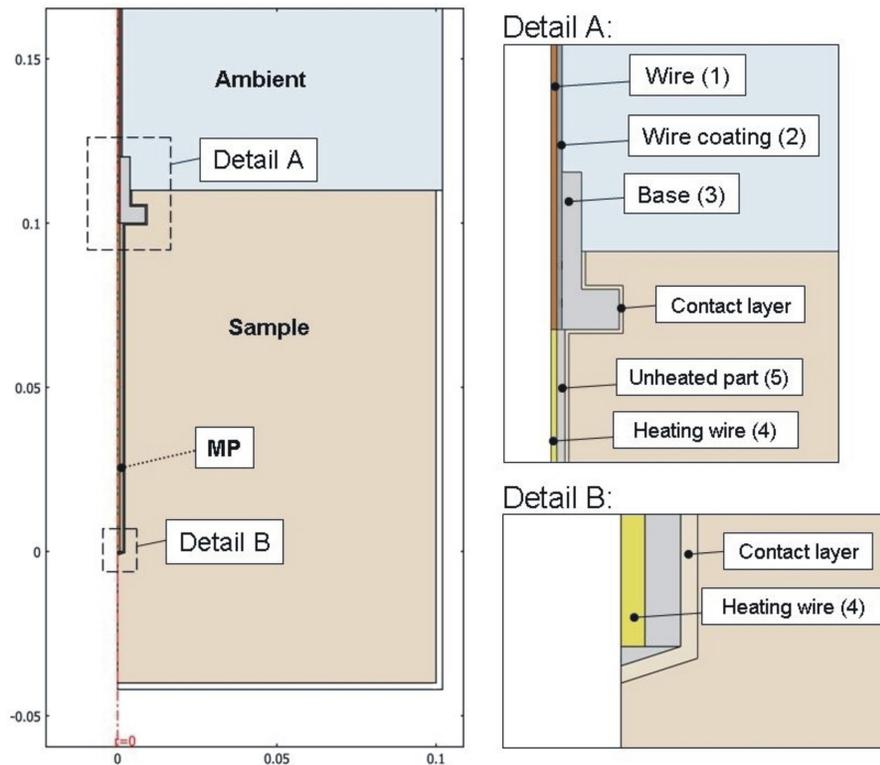


Fig. 16. Model of the LNP03-sensor (short thick needle) embedded in a sample.

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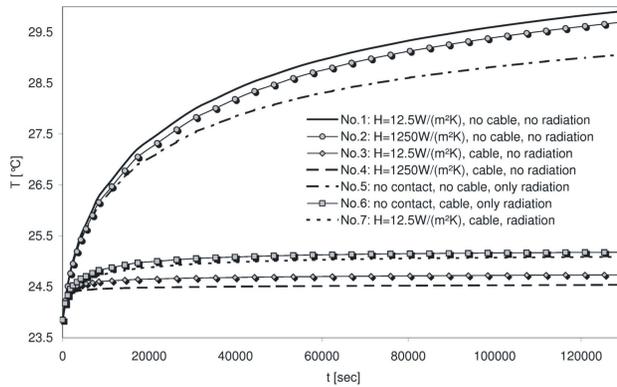
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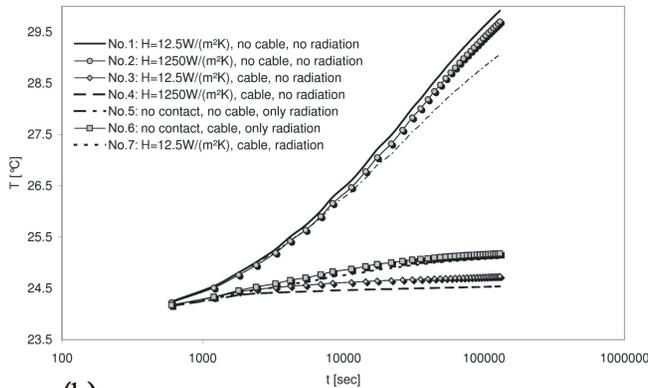
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(a)



(b)

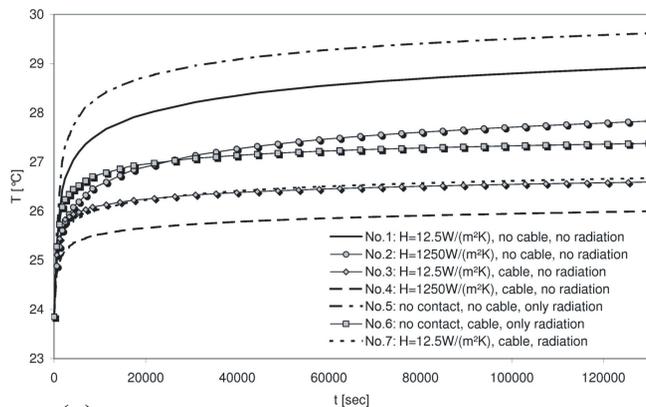
Fig. 17. Temperature response of the LNP03-sensor (short thick needle) at the measurement point due to heating in a very low conductivity sample with $\lambda = 0.002 \text{ W m}^{-1} \text{ K}^{-1}$. **(a)** Temperature versus time on a linear time scale. **(b)** Temperature versus time on a logarithmic time scale.

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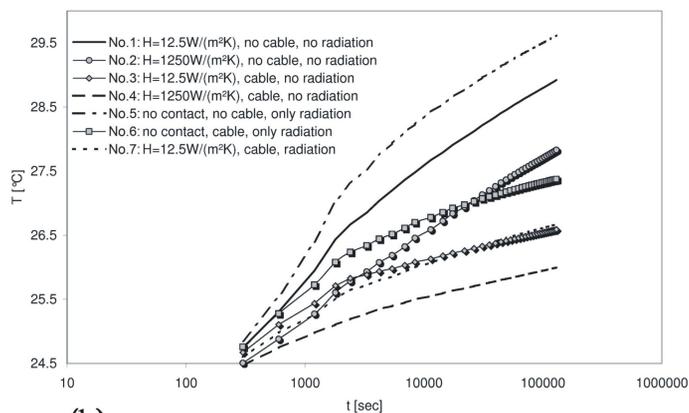


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(a)



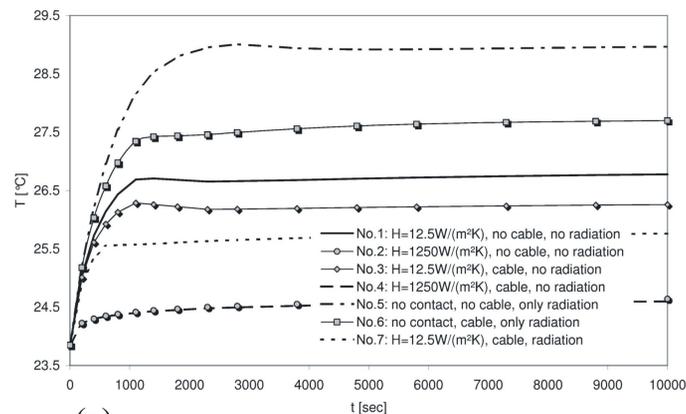
(b)

Fig. 18. Temperature response of the LNP03-sensor (short thick needle) at the measurement point due to heating in a low conductivity sample with $\lambda = 0.02 \text{ Wm}^{-1} \text{ K}^{-1}$. **(a)** Temperature versus time on a linear time scale. **(b)** Temperature versus time on a logarithmic time scale.

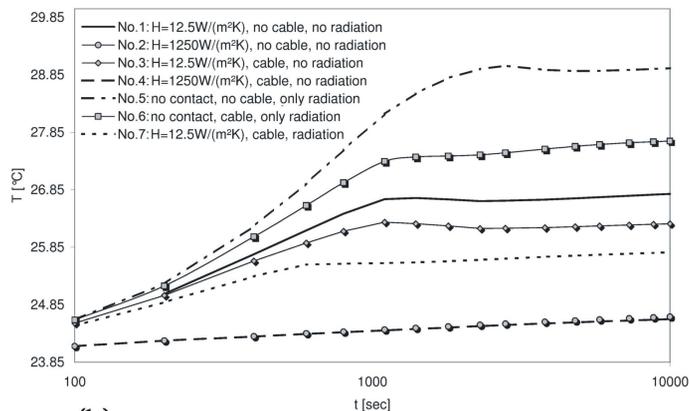
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(a)



(b)

Fig. 19. Temperature response of the LNP03-sensor (short thick needle) at the measurement point due to heating in a moderate conductivity sample with $\lambda = 0.2 \text{ Wm}^{-1} \text{ K}^{-1}$. **(a)** Temperature versus time on a linear time scale. **(b)** Temperature versus time on a logarithmic time scale.

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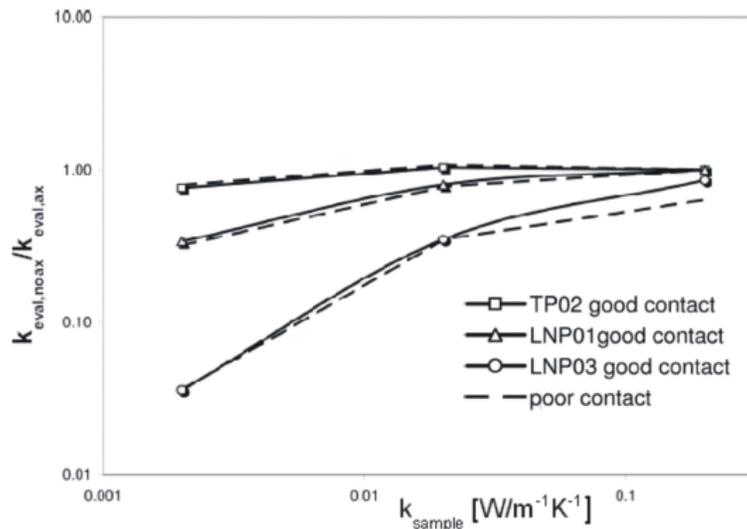


Fig. 20. Ratio of the conductivities determined from the measurement curves, obtained for scenarios including and not including axial heat flow, versus the preset sample conductivity. The continuous lines stand for good contact between sensor and sample and dashed lines for poor contact.

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